Japanese Patent (Kokoku) Publication NO. 58-58123

(Translation)

Japanese Patent (Kokoku) Publication for Opposition No. 58-58123

Publication for Opposition Date: December 23, 1983
Application Number: 56-10439
Filing Date: January 26, 1981
Laid-Open Publication Number: 57-122907
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Inventors: Masao ABE et al.

Gas Separation Film

Claims

A gas separation film, consisting of poly(urethane/disiloxane) having a repeating unit represented by general formula:

(wherein R^1 is a divalent aliphatic group or aromatic group, R^2 is independently a monovalent alkyl group or aromatic group, and n is an integer of 1 through 4).

Detailed Description of the Invention

The present invention relates to a gas separation film consisting of polyurethane including a disiloxane structure.

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Recently, gas separation, especially oxygen enrichment of air by an organic polymer film has been a subject of attention from the viewpoint of saving rescurces and energy. Conventionally known films for oxygen enrichment have an excessively low transmission speed of oxygen or an excessively small transmission coefficient ratio relative to nitrogen, and therefore are not suitable for oxygen enrichment on an industrial scale. For example, polydimethyl siloxane has an oxygen transmisnota coefficient in the order of acm2(STP) cm/cm2 sec cmHg, which is the highest among the coefficients of the conventionally known polymer, films. However, polydimethyl siloxane, which has a transmission coefficient ratio relative to nitrogen of about 2 at most, is inferior in the selective transmittance or separability of oxygen, and thus requires a great number of treatment steps in order to produce oxygen at a high concentration. Therefore, polydimethyl siloxane is not practical in terms of both apparatus requirements and costs. A polydimethyl siloxane film also has a low mechanical strength, and thus needs to be relatively thick. For this reason, the transmission speed of polydimethyl siloxane film cannot be increased although the transmission coefficient is large.

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Accordingly, Japanese Patent Publication for Opposition No. 47-51715 proposes an oxygen enrichment film formed of polyvinyl trimethylsilane. The transmission coefficient ratio of oxygen relative to nitrogen of the film is twice that of polydimethyl siloxane, but the film is inferior in the resistance against chemicals and is likely to be deteriorated by contaminants in the air, oil from pumps or the like. United States Patent

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No. 3,189,662 discloses a polysiloxane-polycarbonate block copolymer. This copolymer is also inferior in the resistance against chemicals due to the polycarbonate structure included.

As a result of active studies on gas separation films which are superior in the selective transmittance of oxygen, resistance against chemicals, mechanical strength and the like, the present inventors found that a gas separation film fulfilling the above-described conditions can be produced by introducing a disiloxane structure into a main chain of polyurethane, and thus made the present invention.

The gas separation film according to the present invention consist of poly(urethane/disiloxane) having a repeating unit represented by general formula:

(wherein R^1 is a divalent organic group, R^2 is independently an alkyl group or aromatic group, and n is an integer of 1 through 4).

In general formula (I), R^1 is a divalent organic group, preferably an aliphatic group or an aromatic group. The aromatic group may be bonded via a hetero atom. Examples of R^1 are expressed by:

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 $(CH_2)_6$ - and the like, where X is a divalent organic bonding group, i.e., a divalent group which can include a valence bond, alkylene group or a hetero atom. Examples of such a divalent group are $-CH_2$ -, $-C(CH_3)_2$ -, -O-, -S- and the like.

 R^2 is a monovalent alkyl group or an aromatic group. The alkyl group preferably has a carbon number of 1 through 4. An especially preferable example of R^2 is a methyl group or a phenyl group. A disiloxane structure contains four R^2 , but all the R^2 are not necessarily identical with one another.

Poly(urethane/disiloxane) having a repeating unit represented by general formula (I) is obtained by causing reaction of the following materials in an appropriate organic solvent with the addition of heat:

(1) diisocyanate represented by general formula:

OCN-RI-NCO

(R¹ is identical as the above-described material), and (1i) disiloxane-based diol represented by general formula:

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r;

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(R2 and n are identical as the above-described materials).

In diisocyanate represented by general formula (II), R¹ is an above-described material. Exemplary preferable diisocyanates include tolylenediisocyanate, phenylenediisocyanate, diphenylmethanediisocyanate, diphenylpropanediisocyanate, diphenyletherdiisocyanate, naphthalenediisocyanate, hexamethylenediisocyanate, and the like.

In disiloxane-based diol represented by general formula (III), R² and n are above-described materials, and can be obtained by a generally known method. The materials represented by general formula (III) are disclosed in United States Patent No. 2,527,591 where n=1, in J. Org. Chem. 25, 1637 (1950) where n=2 and 3, and in United States Patent No. 3,083,219 where n=4.

Used as a reaction solvent for causing reaction of diisocyanate and disiloxane is a material which dissolves both of the materials, is inert to these materials, and dissolves the poly(urethane/disiloxane) to be produced. Exemplary preferable reaction solvents include apportic polar organic solvents such as dimethylsulfoxide, N-methyl-2-pyrrolidone, N,N-dimethylacetoamide, N,N-dimethylformamide and the like. These materials can be used independently or as a mixture of two or more. Pref-

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erably, a mixed solvent of the above-mentioned solvent and an aliphatic or alicyclic ketone, such as methyl ethyl ketone, methyl isobutyl ketone, cyclohexanone, or the like is used. Generally, diisocyanate is difficult to be dissolved in the aprotic polar organic solvent, but can be reacted with diol in a homogenous system or a semi-homogenous system by using a mixed solvent with ketone.

The amount of solvent is not specifically limited, but the solvent is used so that the total amount of disocyanate and disiloxane-based diol is 10 to 50% by weight, preferably 20 to 40% by weight. The temperature of polymerization is usually in the range of 50 to 150°C, and the time period required for the reaction is usually several to several tens of hours. In order to produce a high molecular weight polymer, diisocyanate is used in an amount of a 2 to 45 mol% excess with respect to disiloxane-based diol.

The poly(urethane/disiloxane) produced in this manner usually has a logarithmic viscosity of 0.4 to 1.2, and can be formed into a tough film. The polymer is inert to almost all the organic solvents except for the polar solvents described above as examples of polymerization solvents and some cyclic ethers such as tetrahydrofuran, and thus has a very excellent resistance against chemicals.

The gas separation film according to the present invention can be produced by various methods, but is usually produced in the following manner. Poly(urethane/disiloxane) is dissolved in a solvent for

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film liquid to form a uniform film liquid, and the film liquid is caused to flow over an appropriate support to coat the support with the film liquid. Then, the support coated with the film liquid is heated to vaporize the solvent, thus obtaining a uniform film.

The film preferably has a minimum possible thickness in order to increase the transmission speed of the gas but preferably has a maximum possible thickness in terms of mechanical strength. In consideration of these factors, the film thickness is preferably 0.05 to 30 μm . Accordingly, the concentration of the polymer in the film liquid is 10% by weight or less.

Preferably used as the solvent for film liquid is an aprotic polar organic solvent such as dimethylsulfoxide, N-methyl-2-pyrrolidone, N, N-dimethylacetoamide, dimethylformamide or the like, as in the case of a polymerization solvent. Tetrahydrofuran is also preferable as the solvent for film liquid since it dissolves the poly(urethane/disiloxane) polymer satisfactorily. necessary, a mixed solvent of the aprotic organic solvent and tetrahydrofuran is also used. The temperature at which the film liquid is heated after being applied to the support varies in accordance with the type of the film liquid. When an aprotic polar organic solvent is used, the temperature is 80 to 140°C, preferably 100 to By an especially preferable method, after the solvent is vaporized almost entirely by a temperature in the above-mentioned range, the solvent is heated to about 150°C to be completely vaporized. Tetrahydrofuran which is used as the solvent for film liquid can be va-

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porized at room temperature, and thus a uniform film can be easily produced.

As described above, the gas separation film according to the present invention is formed of polyurethane having a disiloxane structure in a main chain. Owing to the combination of the relatively high oxygen transmission speed of the disiloxane structure, and the excellent selective transmittance of oxygen and the excellent resistance against chemicals of the polyurethane structure, the gas separation film according to the present invention is especially preferable to oxygen enrichment. Due to the great mechanical strength, the gas separation film according to the present invention is optimum for oxygen enrichment of, for example, air, on an industrial scale. The present invention is also applicable for separation of other types of gas.

Hereinafter, examples of the present invention will be described, but the present invention is not limited to these examples. In the following examples, the transmission coefficient P of gas is obtained at 25°C by a high vacuum method, and the separation coefficient α is obtained from the transmission coefficient of the gas/transmission coefficient of nitrogen (P_{N2}) at 25°C.

Example 1

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A dimethylsulfoxide (27 g) solution of bis(hydroxyethyl)tetramethyldisiloxane (8.9 g, 0.040 mol) was added to a methyl isobutyl ketone (120 g) solution of diphenylmethanediisocyanate (13.0 g, 0.052 mol), and heated while being stirred. The viscosity was gradually increased. The reaction was performed

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at 100°C for 5 hours, thus obtaining a very viscous solution. The solution was put into a great amount of water to deposit a polymer, which was pulverized in water. After the resultant material was left overnight, the polymer was filtered and vacuum-dried at 80°C for 10 hours. The resultant polymer had a repeating unit represented by general formula (I), where

$$R^2 = - \bigcirc - CH_2 - \bigcirc - .$$

 R^2 =CH₂ and n=2, and a logarithmic viscosity of 0.88 (N-methyl-2-pyrrolidone, 30°C, 0.5 g/dl; hereinafter, the logarithmic viscosity is measured under the same conditions).

A 5% by weight tetrahydrofuran solution was formed including the polymer and caused to flow over a tinplated board. Then, the board was left at room temperature for 3 days to vaporize the solvent. Then, tin was dissolved in mercury into amalgam, thereby obtaining a uniform polymer film having a thickness of 10 μ m. The gas transmittance of the polymer film was measured by a high vacuum method. The results are shown in Table 1.

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Table 1

Gas transmittance of poly(urethane/disiloxane) film

Gas	Transmittance coefficient P (CC(STP) · cm/cm² · sec · cmHg)	Separation
Hydrogen	2.2×10 ⁻⁹	coefficient a
Helium	2.1×10°	45
Carbon dioxide	1.4×10 ⁻⁹	30
Oxygen	2.8×10 ⁻¹⁰	6
Argon	1.8×10 ⁻¹⁰	4
Nitrogen	4.7×10 ⁻¹¹	1

As a comparative example, a polyurethane film was prepared in the same manner as in example 1 except that ethyleneglycol (2.7 g, 0.043 mol) was used instead of bis(hydroxyethyl)tetramethyldisiloxane. The gas transmittance of the polyurethane film is shown in Table 2.

Table 2

Transmittance coefficient P (CC(STP) cm/cm ² sec cmHq)	
	coefficient a
2.4×10 ⁻¹⁰	308
3 8×10 ⁻¹⁰	490
	430
2.7×10 ⁻¹¹	35
5 - 8×10 ⁻¹²	7
0.0420	,
2.0×10 ⁻¹²	3
7 8×10-13	1
	5.8×10 ⁻¹²

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As can be appreciated from the above-described results, the poly(urethane/disiloxane) film according to the present invention increases the selective transmittance of oxygen by 50 times while maintaining a high separation coefficient of oxygen relative to nitrogen. Furthermore, the film according to the present invention is insoluble in almost all the organic solvents except for the aprotic polar organic solvents and tetrahydrofuran, and thus has an excellent resistance against chemicals. Moreover, the film is tough and has a sufficient mechanical strength as indicated by a strength against rupture of 740 kg/cm² and an elongation at rupture of 4% which were measured at a tensile rate of 50 mm/min. and a temperature of 25°C.

Example 2

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A poly(urethane/disiloxane) polymer was prepared in the same manner as in example 1 except that 2,4tolylenediisocyanate (7.5 g, 0.043 mol) was used instead of diphenylmethanediisocyanate and bis(hydroxypropyl)tetramethyldisiloxane (10.0 g, 0.040 mol) was used instead of bis(hydroxyethyl)tetramethyldis1loxane. The resultant polymer is represented by the above general formula, where

$$R^1 = - \bigcirc - CH_s$$

 R^2 =CH₂ and n=3, and has a logarithmic viscosity of 0.76. A film having a thickness of 15 μ m was prepared based on the polymer in the same manner as in example 1. The film had a transmission coefficient of oxygen of 3.0×1.0⁻¹⁶

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CC(STP)·cm/cm²·sec·cmHg and a separation coefficient of 5.7.

Example 3

A polymer was prepared in the same manner as in example 1 except that hexamethylenediisocyanate was used instead of diphenylmethanediisocyanate and that bis(hydroxybutyl)tetraphenyldisiloxane was used instead of bis(hydroxyethyl)tetramethyldisiloxane. The resultant polymer is represented by general formula (I) where R^{1} =-(CH₂)₆, R^{2} =-C₆H₅-, n=4, and has a logarithmic viscosity of 0.61. A film prepared based on the polymer in the same manner as in example 1 had a transmission coefficient of oxygen of 8.2×1.0^{-10} CC(STP)·cm/cm²·sec·cmHg and a separation coefficient of 3.2.

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Detailed Description of the Invention

The present invention relates to a gas separation film consisting of polyurethane including a disiloxane structure.

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Recently, gas separation, especially oxygen enrichment of air by an organic polymer film has been a subject of attention from the viewpoint of saving resources and energy. Conventionally known films for oxygen enrichment have an excessively low transmission speed of oxygen or an excessively small transmission coefficient ratio relative to nitrogen, and therefore are not suitable for oxygen enrichment on an industrial scale. example, polydimethyl siloxane has an oxygen transmisorder of the in the coefficient 8cm²(STP)·cm/cm²·sec·cmHg, which is the highest among the coefficients of the conventionally known polymer films. However, polydimethyl siloxane, which has a transmission coefficient ratio relative to nitrogen of about 2 at most, is inferior in the selective transmittance or separability of oxygen, and thus requires a great number of treatment steps in order to produce oxygen at a high concentration. Therefore, polydimethyl siloxane is not practical in terms of both apparatus requirements and costs. A polydimethyl siloxane film also has a low mechanical strength, and thus needs to be relatively thick. For this reason, the transmission speed of polydimethyl siloxane film cannot be increased although the transmission coefficient is large.

Accordingly, Japanese Patent Publication for Opposition No. 47-51715 proposes an oxygen enrichment film formed of polyvinyl trimethylsilane. The transmission coefficient ratio of oxygen relative to nitrogen of the film is twice that of polydimethyl siloxane, but the film is inferior in the resistance against chemicals and is likely to be deteriorated by contaminants in the air, oil from pumps or the like. United States Patent

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No. 3,189,662 discloses a polysiloxane-polycarbonate block copolymer. This copolymer is also inferior in the resistance against chemicals due to the polycarbonate structure included.

As a result of active studies on gas separation films which are superior in the selective transmittance of oxygen, resistance against chemicals, mechanical strength and the like, the present inventors found that a gas separation film fulfilling the above-described conditions can be produced by introducing a disiloxane structure into a main chain of polyurethane, and thus made the present invention.

The gas separation film according to the present invention consist of poly(urethane/disiloxane) having a repeating unit represented by general formula:

O O
$$R^{2}$$
 R^{2}

|| || || || ||
-OCNH-R¹-NHCO(CH₂)_n Si-O-Si(CH₂)_n- (|)
|| || ||
|| R² R²

(wherein R^1 is a divalent organic group, R^2 is independently an alkyl group or aromatic group, and n is an integer of 1 through 4).

In general formula (I), R^1 is a divalent organic group, preferably an aliphatic group or an aromatic group. The aromatic group may be bonded via a hetero atom. Examples of R^1 are expressed by:

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 $(CH_2)_6$ - and the like, where X is a divalent organic bonding group, i.e., a divalent group which can include a valence bond, alkylene group or a hetero atom. Examples of such a divalent group are $-CH_2$ -, $-C(CH_3)_2$ -, -0-, -S- and the like.

 R^2 is a monovalent alkyl group or an aromatic group. The alkyl group preferably has a carbon number of 1 through 4. An especially preferable example of R^2 is a methyl group or a phenyl group. A disiloxane structure contains four R^2 , but all the R^2 are not necessarily identical with one another.

Poly(urethane/disiloxane) having a repeating unit represented by general formula (I) is obtained by causing reaction of the following materials in an appropriate organic solvent with the addition of heat:

(i) disocyanate represented by general formula:

OCN-R1-NCO

(R¹ is identical as the above-described material), and (ii) disiloxane-based diol represented by general formula:

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(R² and n are identical as the above-described materials).

In diisocyanate represented by general formula (II), R¹ is an above-described material. Exemplary preferable diisocyanates include tolylenediisocyanate, phenylenediisocyanate, diphenylmethanediisocyanate, diphenylpropanediisocyanate, diphenyletherdiisocyanate, naphthalenediisocyanate, hexamethylenediisocyanate, and the like.

In disiloxane-based diol represented by general formula (III), R^2 and n are above-described materials, and can be obtained by a generally known method. The materials represented by general formula (III) are disclosed in United States Patent No. 2,527,591 where n=1, in J. Org. Chem. 25, 1637 (1950) where n=2 and 3, and in United States Patent No. 3,083,219: where n=4.

Used as a reaction solvent for causing reaction of diisocyanate and disiloxane is a material which dissolves both of the materials, is inert to these materials, and dissolves the poly(urethane/disiloxane) to be produced. Exemplary preferable reaction solvents include aprotic polar organic solvents such as dimethylsulfoxide, N-methyl-2-pyrrolidone, N,N-dimethylacetoamide, N,N-dimethylformamide and the like. These materials can be used independently or as a mixture of two or more. Pref-

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erably, a mixed solvent of the above-mentioned solvent and an aliphatic or alicyclic ketone, such as methyl ethyl ketone, methyl isobutyl ketone, cyclohexanone, or the like is used. Generally, diisocyanate is difficult to be dissolved in the aprotic polar organic solvent, but can be reacted with diol in a homogenous system or a semi-homogenous system by using a mixed solvent with ketone.

The amount of solvent is not specifically limited, but the solvent is used so that the total amount of disocyanate and disiloxane-based diol is 10 to 50% by weight, preferably 20 to 40% by weight. The temperature of polymerization is usually in the range of 50 to 150°C, and the time period required for the reaction is usually several to several tens of hours. In order to produce a high molecular weight polymer, diisocyanate is used in an amount of a 2 to 45 mol% excess with respect to disiloxane-based diol.

The poly(urethane/disiloxane) produced in this manner usually has a logarithmic viscosity of 0.4 to 1.2, and can be formed into a tough film. The polymer is inert to almost all the organic solvents except for the polar solvents described above as examples of polymerization solvents and some cyclic ethers such as tetrahydrofuran, and thus has a very excellent resistance against chemicals.

The gas separation film according to the present invention can be produced by various methods, but is usually produced in the following manner. Poly(urethane/disiloxane) is dissolved in a solvent for

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film liquid to form a uniform film liquid, and the film liquid is caused to flow over an appropriate support to coat the support with the film liquid. Then, the support coated with the film liquid is heated to vaporize the solvent, thus obtaining a uniform film.

The film preferably has a minimum possible thickness in order to increase the transmission speed of the gas but preferably has a maximum possible thickness in terms of mechanical strength. In consideration of these factors, the film thickness is preferably 0.05 to 30 μ m. Accordingly, the concentration of the polymer in the film liquid is 10% by weight or less.

Preferably used as the solvent for film liquid is an aprotic polar organic solvent such as dimethylsulfoxide, N-methyl-2-pyrrolidone, N, N-dimethylacetoamide, dimethylformamide or the like, as in the case of a polymerization solvent. Tetrahydrofuran is also preferable as the solvent for film liquid since it dissolves the poly(urethane/disiloxane) polymer satisfactorily. necessary, a mixed solvent of the aprotic organic solvent and tetrahydrofuran is also used. The temperature at which the film liquid is heated after being applied to the support varies in accordance with the type of the film liquid. When an aprotic polar organic solvent is used, the temperature is 80 to 140°C, preferably 100 to By an especially preferable method, after the solvent is vaporized almost entirely by a temperature in the above-mentioned range, the solvent is heated to about 150°C to be completely vaporized. Tetrahydrofuran which is used as the solvent for film liquid can be va-

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porized at room temperature, and thus a uniform film can be easily produced.

As described above, the gas separation film according to the present invention is formed of polyurethane having a disiloxane structure in a main chain. Owing to the combination of the relatively high oxygen transmission speed of the disiloxane structure, and the excellent selective transmittance of oxygen and the excellent resistance against chemicals of the polyurethane structure, the gas separation film according to the present invention is especially preferable to oxygen enrichment. Due to the great mechanical strength, the gas separation film according to the present invention is optimum for oxygen enrichment of, for example, air, on an industrial scale. The present invention is also applicable for separation of other types of gas.

Hereinafter, examples of the present invention will be described, but the present invention is not limited to these examples. In the following examples, the transmission coefficient P of gas is obtained at 25°C by a high vacuum method, and the separation coefficient α is obtained from the transmission coefficient of the gas/transmission coefficient of nitrogen (P_{N2}) at 25°C.

Example 1

A dimethylsulfoxide (27 g) solution of bis(hydroxyethyl)tetramethyldisiloxane (8.9 g, 0.040 mol) was added to a methyl isobutyl ketone (120 g) solution of diphenylmethanediisocyanate (13.0 g, 0.052 mol), and heated while being stirred. The viscosity was gradually increased. The reaction was performed

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at 100°C for 5 hours, thus obtaining a very viscous solution. The solution was put into a great amount of water to deposit a polymer, which was pulverized in water. After the resultant material was left overnight, the polymer was filtered and vacuum-dried at 80°C for 10 hours. The resultant polymer had a repeating unit represented by general formula (I), where

$$R^1 = -\bigcirc - CH_2 -\bigcirc -$$

 R^2 =CH₂ and n=2, and a logarithmic viscosity of 0.88 (N-methyl-2-pyrrolidone, 30°C, 0.5 g/dl; hereinafter, the logarithmic viscosity is measured under the same conditions).

A 5% by weight tetrahydrofuran solution was formed including the polymer and caused to flow over a tinplated board. Then, the board was left at room temperature for 3 days to vaporize the solvent. Then, tin was dissolved in mercury into amalgam, thereby obtaining a uniform polymer film having a thickness of 10 μ m. The gas transmittance of the polymer film was measured by a high vacuum method. The results are shown in Table 1.

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Table 1

Gas transmittance of poly(urethane/disiloxane) film

Gas	Transmittance coefficient P	Separation
	(CC(STP) · cm/cm ² · sec · cmHg)	coefficient a
Hydrogen	2.2×10 ⁻⁹	47
Helium	2.1×10 ⁻⁹	45
Carbon dioxide	1.4×10 ⁻⁹	30
Oxygen	2.8×10 ⁻¹⁰	6 ;
Argon	1.8×10 ⁻¹⁰	4
Nitrogen	4.7×10 ⁻¹¹	1

As a comparative example, a polyurethane film was prepared in the same manner as in example 1 except that ethyleneglycol (2.7 g, 0.043 mol) was used instead of bis(hydroxyethyl)tetramethyldisiloxane. The gas transmittance of the polyurethane film is shown in Table 2.

Table 2

CC(STP) · cm/cm ² · sec · cmHg) 2.4×10 ⁻¹⁰ 3.8×10 ⁻¹⁰	coefficient α 308 490
3.8×10 ⁻¹⁰	490
2.7×10 ⁻¹¹	35
5.8×10 ⁻¹²	7
2.0×10 ⁻¹²	3
7.8×10 ⁻¹³	1
	5.8×10 ⁻¹² 2.0×10 ⁻¹²

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As can be appreciated from the above-described results, the poly(urethane/disiloxane) film according to the present invention increases the selective transmittance of oxygen by 50 times while maintaining a high separation coefficient of oxygen relative to nitrogen. Furthermore, the film according to the present invention is insoluble in almost all the organic solvents except for the aprotic polar organic solvents and tetrahydrofuran, and thus has an excellent resistance against chemicals. Moreover, the film is tough and has a sufficient mechanical strength as indicated by a strength against rupture of 740 kg/cm² and an elongation at rupture of 4% which were measured at a tensile rate of 50 mm/min. and a temperature of 25°C.

Example 2

A poly(urethane/disiloxane) polymer was prepared in the same manner as in example 1 except that 2,4tolylenediisocyanate (7.5 g, 0.043 mol) was used instead diphenylmethanediisocyanate and that bis(hydroxypropyl)tetramethyldisiloxane (10.0 g,0.040 mol) was used instead bis(hydroxyethyl)tetramethyldisiloxane. The resultant polymer is represented by the above general formula, where

$$R^{1} = - \bigcirc - CH_{8},$$

 R^2 =CH₂ and n=3, and has a logarithmic viscosity of 0.76. A film having a thickness of 15 μ m was prepared based on the polymer in the same manner as in example 1. The film had a transmission coefficient of oxygen of 3.0×1.0^{-10}

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CC(STP)·cm/cm²·sec·cmHg and a separation coefficient of 5.7.

Example 3

A polymer was prepared in the same manner as in example 1 except that hexamethylenediisocyanate was used instead of diphenylmethanediisocyanate and that bis(hydroxybutyl)tetraphenyldisiloxane was used instead of bis(hydroxyethyl)tetramethyldisiloxane. The resultant polymer is represented by general formula (I) where $R^1=-(CH_2)_6$, $R^2=-C_6H_5-$, n=4, and has a logarithmic viscosity of 0.61. A film prepared based on the polymer in the same manner as in example 1 had a transmission coefficient of oxygen of 8.2×1.0^{-10} CC(STP)·cm/cm²·sec·cmHg and a separation coefficient of 3.2.

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RI

R*

(但し、R1 は2個の脂肪放送又は芳香族物、R8 はそれぞれ設立に1個のアルキル基又は芳香族帯、nは1~4の竪数を示す。) で表わされる繰返し単位を有するがり(フレタン/ジシロチテレ)からなるととも特徴とする気体分散腫。

発明の耳器な説明

本発明はジシロキサン構造を含むポリウレタン

からなる気体分離膜に関する。

近年、省資源、省エネルギーの観点から有機重 合体膜による気体分離、等に空気の酸素富化が注 日されているが、従来知られている酸果室化用膜 は歌影の透過速度が小さすぎ、或いは電影に対す る酸素の透過係数比が小さいため、工業的な規模 で数素害化を行たりには逞しない。例えばポリジ メテルシロネサンは酸素の透過保敷が10 🗝 👊 (STP)・caytal・sec・cally 台であって、従来 知られている重合体傷のなかでは最大でもるが。 電素に対する透過係数比が積々る程度であって。 要素の選択透過性又に分離性に劣り、高級度の数 未も得ようとければ多数の映処理を受けることと なり、禁食、費用のいずれの点からも爽用的でな い。また、この騒は眼球的強度が小さく、比較的 厚い旗を用いる必要があり、従つて、透過係数は 大きくとも、透過速度を大きくすることができた

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このため母公昭 4 7 + 5 1 7 1 5 号公報にはポリピニルトリメテルションからなる職業官化質が提案されてかり、壁楽の電景に対する透透係数比はポリジメテルシロキサンの約 2 倍に改容されているが、耐薬品性に劣り、空気中の汚染物質。ポンプ調からの信号により劣化しやすい欠点がある。また、米国特許解 3 1 8 9 6 6 2 号にはポリシロキサンーボリカーボネートプロック共重合体が解示されているが、ポリカーボネート構造を含むために、ポリピニルトリメテルシラン膜同様に耐薬品性に劣る。

20 本発明者もは酸素の選択透過性、耐薬品性、機 機的強度等にすぐれる気体分配度について観念研究を重ねた結果、ポリウレタンの主盤中にジシロ キャン構造を導入することにより上記受水に通う 気体分離臓を得ることができることを見出し、本 35 効明に至つたものである。

本発明による気体分離膜は一般式

(但し、Riは2価の有限基、Riはそれぞれ独 10 ★ 一致式∏にかいて、Riは2価の有機基、好まし 立ドアルキル高叉は芳香灰基、ロはエー4の整数 七示す。)

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で使わるれる鏡返し単位を右するポリくウレクン ノジシロキサン)からなることを特徴とする。

くは脂肪製造又は芳香製造であり、ここに芳香族 遊はヘテロ原子を介して総合されていてもよい。 從つて、これ6の具体例として

(CSto)a一等を挙げるととがです。ことにX は2個の有機結合基、即ち、原子価値合、アルキ レン基又はヘテロ原子を含んでよい2個基でもつ て、具体例として一CH2-,-C(CH3)2-, 25 一〇一,一8一等を挙げるととが言る。

R^a は1価のアルキル基又は芳香族基である。 アルキル当は好さしくは昃未敢が 1 ~4 である。 R* の特に好きしい具体例はメテル基又はフェニ ル基である。ジシロ中サン構造は4つのR5 を有 め するが。すべての日・が同一である必要はない。

一般式(1)で表わざれる構返し単位を有するポリ (ウレタン/ジシロキサン)は一般式

(R1 は前紀と同じである。) で表わされるタイソシアネートと、一般式

(但し、 RE 及びnは前記と同じである。)

で表わされるジンロキサン系ジォールとを適宜の 有機器剤中ドで加熱、反応させることによって発 られる。

上記一般式印で表わされるツィソシアネートに かいて、RI は前配したとかりであり、好さしい ジイソンアネートの具体例としてトリレンジィン ンアネート、フエニレンジインシアネート、ツァ エニルメタンジイソンアネート、ジフエエルプロ ペンジイソシアネート、 シフエニルエーテルジイ ソンアネート。ナフタレンジイソシアネート、ヘ キサメテレンダイソシアネート等を挙げることが てきる。

さた、上記一般式伽で扱わされるリシロキサン 系ジオールにかいて、RF 及びの社前配したとか りてもり、一般に既に知られている方法によって ・得ることができる。即ち、ュー1の場合は米国特 許第2527891号に、ロー2及び3の場合は J.Org. Chm. 25, 1687 (1950)K. また、ロニ4の場合は米国特許第3083218 サド発示されている。

上記ジイソシアキートとジシロキサンとせ反応 をせるための反応適効は好きしくは、これら質者 を共に帰郷し得ると共に、これらに対して不活性

であり、且つ、生成するポリ(ウレャンノジシロ キサン 3 富合体をも磨除し得るものが用いられる。 好もしい有機痞剤の具体例としてはシメナルエル ホキッド、パーメチャー2ーピロリドン、パ・パ ージメテルアセトアミド、N。N-ジメテルホル ミ AT!ド等の非プロトン性値性有機溶剤が挙げられ、 一種又は二種以上の退合物が用いられ、好をしく は上紀移剤とメチルエナルケトン、メチルメソブ テルケトン、シタロへキサノン郷の脂肪質、脂環 族ケトン類との国合帝別が用いられる。一般にジ 10 イソシアネートは上記非プロトン性医性有機添熟 に庭習性であるが、ケトン親との虚合管剤を用い ることによりジオールとの反応を均一系又は均一 系K近い状態で行なうととができる。

格剤の使用量は特に制限されないが、ジイソシ 18 アネートとジンロキサン系ジオールとの合計量が 10~50重量気、好せしくは20~40重量気 となるように用いられる。重合反応の良度は通常、 50~150℃の範囲であり、反応に要する時間 は過常、数時間~数十時間である。尚、海分子量 30 械的強度も大きいので、例えば空気の歌楽富化の の重合体を得るには、ツシロキサン系ジナールに 対してジイソシアネートを2~45モル多程批通 乳に用いるのがよい。

このようにして得られるポリ(クレクン/ジン ロチケン)は通常。 0.4 ~1.2 の対极粘度を有し、25 強靱な異に形成するととができる。との重合体は 2000年前として例示したような前距医性溶剤 及びテトラヒドロフランのような一部の環状エー テルを除き、ほとんどの有機溶剤に不活性でもつ て、何めてナぐれた耐楽品性を有している。 30

本発明による気体分離膜は穏々の方法によって 製造することができるが、普通は、上記がり(ウ レダンノジシロキサン)を製度液溶剤に密解して 特一な製ی放とし、これを建立の支持基材に洗延 **歯布した後、加熱処理して密剤を蒸発させて均質 as** な観とする。

気体の透過速度を大きくするためには進厚は海 い程序をしいが、一方、磁線的強度の点からは原 い方が好さしく、これらの観点から健康は 0.0 5 一30 xが望ましい。使って、製験核の宣合体数 40 た宣合体は前辺一般式(1)化かいて 配は10重量多以下がよい。

製填液溶剤は重合反応器剤を同様にジメチルス · ルホキシド、Nーメナルー2ーピロリドン、N。 Nージメチルアセトアミド、N.Nージメチルホ

ルムアミド等の非プロトン性征性有機器前が好せ しい。 また。ナトラヒドロフランもぷり(ウレタ ングシャキテン)重合体をより影響するので製 腱核溶剤として好道である。必要ならば上記非ブ ロトン性有极溶剤及びアトラヒドロフランの混合 避明を用いられる。 製膜液を支持基材に塗布後、 加熱する風度は製農液密剤にもよるが、上記非ブ ロトン性極性有機必須の場合には80~140℃、 好さしくは100~120℃である。 特に好まし くはこのような健康範囲で移列のほとんど蒸発さ **仕大後。150℃程度に昇進して溶剤を完全に蒸** 元させる。製製液溶剤としてテトラヒドロフラン を用いた場合には常温でとれを蒸発させることが でき、均質な裏を容易に得るととができる。

本発明の気体分離膜は以上のように主境にツシ ロチナン構造を介するポリウレクンからなり、ジ シロキテン構造の大きい酸素の透過速度とポリウ レタン構造のすぐれた酸素の選択透過性、耐薬品 性と相俟つて特に酸素富化に好達であり、更に機・ 工業的実施に最適である。しかしながら、他の気 体温合物の減分能への使用を続けるものではない。

以下に本発明の実施例を挙げるが、本発明はと れらに限定されるものではない。尚、以下の突然 例にかいて、気体の透過係数Pは25℃で高安空 法によう求めたものであり、分離係数では25℃ にかける当該気体の透過係数/音素の透過係数 (PNs)から水めたものである。

実施例 1

ピス(ヒドヨキシステル)テトラメテルジシロ チサン(8.8 分、 0.0 4 0 モル) のジメテルスル ホキシド(279」薔薇をツフエエルメタンジイ ソンアネート(1308、Q052モル)のメナ ルイソプテルケトン(120分)密放に加え、橙 押下に加思した。徐々に粘度が上昇した。100 ての設定で5時間反応させて非常に粘視な溶液を. 得た。この形骸を大量の水中に投じ、金合体を折 出させ、水中で発砕した。一夜放置後、重合体を・ 产別し、80℃で10年間食空乾燥した。得られ

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であつた(Nーメチルー2ーピロリドン、30℃。 wB脇放置して密刳を蒸発させ、次にスメを水低で 0.5 8/dL、以下同じ。)。

との重合体を5重量労のナトラヒドロフラン郡 放とし、スポメッキゼ上に放逐した径。金温で3ヵ

アマンガムにして密かし、厚み10gの均質な量 全体語を得た。との重合体質の気体透過性を高真 空法化で開定し、結果を第1表に示す。

ポリ(ウレタシノジツロキサン)器の気体透過性

気 体	选通係数P (CC(STP)∗am/cm²⋅sec⋅amHar)	分產係数点
水 套	2.3×10→	4.7
ヘリウム	21×10-	4.5
二酸化炭素	1.4 × 1 0> -	8 0
政士	28×10 ⁻¹⁰	. 6
ブルゴン	1.8 × 1 0 -10	4
Q P	4.7 × 1 0 -11	1

上較例として、実施例1にかいてビス(x Fo キシェテル)テトラメチルジシロキサンの代わり たエテレングリコール[279.0043モル] *

*を用いた以外は実施領1と全く阿様にしてポリワ レアン膜を顕製した。とのポリウレテン膜の気体 透過性を第2会に示す。

気 体	透填纸数字 (CC(STP)·cm/cm²·sec-caH?)	分離係数々
水景	24×10~16	308
~594	3.8 × 1 0 -10	490
二酸化炭素	2.7 × 1 0 -13	3.5
歌 裏	5.8 × 1 0 —12	7
アルゴン	20×10-12	3
建 太	7.8 × 1 0 -13	1

以上の結果から、本発明のポリ(ウレタン/ジ 80 ート(7.5 8,00 4 3 モル)を、また、ヒス シロキサン)裏によれば散集の窒素に対する分離 係数を高く維持して、酸素の選択透過性を約50 倍増大させるととができた。更に、本苑明の職は 前紀非プロトン性優性有機溶剤及びテトラヒドロ 25 フランを除くほとんどナペての有根着剤に不溶性 でもつて、耐薬品性に着しくすぐれるほか、引法 速度50四/分、速度28℃化で測定した破断法 度及び放断伸びはそれぞれ 7 4 0 個/og 及び 4 **系であつて、親は強硬で十分な機械的強度を有す 40**

実施例 2

肉体例1にかいてジフェニャメタン ジイソシア ホートの代わりにて。 4ート リレンジイソシアホ

(ヒドロキシエテル)テトラメチルジシロキサン の代わりにヒス(モドロテンプロピル)テトラメ ナルジシロチサン(1008、0.040モル)を 用いた以外は、実施例1と全く同様にして、前記

ロー3であつて、対数粘度 0.76のポリ (.クレタ ンノリシロキサン】重合体を得た。との重合体が 5実施例1と同様にして厚み15』の誰を観叙し た。 酸素の透過係数は 3.0 × 1.0 ~10 CC(STP)・ ca/cal·esc·cally、分類係数は5.7であった。

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実施例 5

突的例1においてツフェニルメタン ジイソシア ネートの代わりにペキサメテレンジイソンアネートを、また、ピス(ヒドロキシエテル)テトラメ テルソシロキサンの代わりにピス(ヒドロキシブ 5 テル)テトラフエニルジンロキサンを用いた以外

は、実施例1と全く阿様にして、前記一般式(I)に かいてR¹=-(CH₂)。R²=-C₆H₃-1。m 4、対数能度 0.6 1 の重合体を視た。この重合体 から実施例1と阿様にして得た原は酸素の透過像 数 8.2 × 1 0 -19 CC(STP)・cm/cm²・sec = cm HP、酸素の分離係数 3.2 であった。

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